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(54) IMPROVEMENTS IN AND RELATING TO THE TREATMENT OF OXIDE PIGMENTS

(71) We, LAPORTE INDUSTRIES LIMITED, a British Company of Hanover House, 14 Hanover Square, London, W1R 0BE, do hereby declare the invention, for which we pray that a patent may be granted to us, and the method by which it is to be performed, to be particularly described in and by the following statement:—

This invention relates to the treatment of oxide pigments, and especially to the treatment of titanium dioxide pigments. It has become well-established practice to coat pigmentary oxide particles with one or more inorganic substances, in order to improve various properties of the pigmentary particles. Thus, for example, the hiding power and dispersibility of pigmentary titanium dioxide is improved by coating the pigment with one or more hydrous oxides. Such coatings also reduce the chemical reactivity of the pigmentary particles and increase the resistance of the particles to attack by light.

Although coated pigments have very desirable properties in some respects, they tend to be somewhat difficult to mill and to filter, and these processing difficulties tend in turn to impair the gloss of the finished pigment, and may also impair its oil absorption value. Further, although it is desirable for some purposes to apply a relatively thick coating to oxide pigments, the problems involved in milling and filtering become increasingly severe as the thickness of the coating increases. Especially great milling difficulties are en-

countered when, in accordance with a previous proposal for improving the photochemical stability of titanium dioxide pigments the coated pigment is baked at an elevated temperature before being milled.

The present invention provides a process for the treatment of an oxide pigment, which comprises forming on the pigment a coating comprising at least one substance selected from hydroxides, hydrous oxides, phosphates and basic sulphates of beryllium, calcium, magnesium, barium, boron, aluminium, silicon, tin, lead, antimony, titanium zirconium, hafnium, niobium, tantalum, zinc, and cerium, and subjecting the coated pigment to hydrothermal pressure treatment by maintaining it at a temperature of at least 50°C. in the presence of liquid water and with a total ambient pressure exceeding one atmosphere.

The hydrothermal pressure treatment in accordance with the invention leads generally to an improvement in the ease of milling of coated oxide pigments. In addition, certain important characteristics of the coated pigment, notably its gloss and oil absorption value, can be improved by the hydrothermal pressure treatment process. Moreover, in some cases, and, in particular, in the case of titanium dioxide pigments having a coating comprising hydrous alumina and hydrous silica, the treatment can have a beneficial effect on the hiding power and photochemical stability of coated oxide pigments.

The oxide pigment may be a chromic oxide



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or iron oxide pigment, but an especially important form of the process of the invention is that in which the oxide pigment is pigmentary titanium dioxide whether obtained from titanium sulphate or from titanium tetrachloride. The titanium dioxide pigment may, for example, be a composite pigment (with calcium sulphate or barium sulphate), or it may be a pigment extended with china clay, talc, silica, or an alumino-silicate. A process for the manufacture of pigmentary titanium dioxide is described in the Complete Specification accompanying our co-pending United Kingdom Application No. 62927/69 (Serial No. 1,335,184).

The hydrothermal pressure treatment must, of course, be carried out in a vessel, for example, an autoclave, in which a superatmospheric pressure can be maintained.

Advantageously, there is liquid water in contact with the coated pigment during the hydrothermal pressure treatment.

Advantageously, the superatmospheric pressure is that pressure obtained when an aqueous mixture including the coated pigment is sealed in a closed vessel and thereafter heated to the desired temperature. If it is desired to increase the total pressure without increasing the temperature, then the pressure may be augmented by introducing a gas into the vessel. Advantageously, any gas introduced into the treatment vessel is air or nitrogen, although any gas may of course be used which does not have a detrimental effect on the properties of the coated pigment.

Preferably, the temperature at which the coated pigment is maintained is at least 150°C. As it is advantageous that part of the water present in the treatment vessel should be in liquid form, the temperature within the treatment vessel is preferably not greater than the critical temperature of water (374°C).

The amount of water in the treatment vessel and the conditions of temperature and pressure therein are advantageously such that substantially the whole of the exposed surface area of the coated pigment is in contact with liquid water.

Preferred phosphates are those of titanium, aluminium, and zirconium.

Preferably, the pigment is coated with one or more substances selected from hydroxides, hydrous oxides, and basic sulphates. The coating may be applied to the pigmentary particles in any suitable manner. Normally, the coating is applied by adding the appropriate surface-treating agent or agents to an aqueous slurry of the pigment. Thus, for example, the coating may be deposited on the pigment by contacting the pigment with an alkaline agent and with an acid-reacting compound of the desired element. Alternatively, the coating may be formed by treating the pigment with an acid-reacting compound of a

selected element and with a basic compound of the same element or of another selected element. Thus, for example, the coating may be the result of treating the pigment with titanium tetrachloride and sodium aluminate.

As an alternative to forming the coating by an acid-base reaction, it may be formed by hydrolysis of a compound of the desired element, for example, by the hydrolysis of titanium tetrachloride.

Advantageously, the coating is formed by precipitating quantities of hydroxides or hydrated oxides of two or more of aluminium, silicon, boron, titanium, antimony, zinc, magnesium, tin, lead, cerium and zirconium into intimate association with the pigment.

The coating may consist of one layer formed by co-precipitation of two or more hydroxides, hydrated oxides, phosphates and/or basic sulphates, or of a plurality of discrete layers, each such discrete layer having been deposited separately. Where the coating consists of a plurality of discrete layers, each layer may consist of a single hydroxide, hydrous oxide, phosphate, or basic sulphate, or some or all of the layers may consist of more than one such compound.

When the oxide pigment is a titanium dioxide pigment the surface coating may be formed, for example, according to the process described in the Provisional Specification accompanying our co-pending United Kingdom Application No. 44717/70. In that process, a first coating of hydrous alumina is formed on the pigment, a part of the resulting coating is dissolved, and a second coating is formed comprising re-precipitated alumina and a hydrous oxide of one or more of the elements titanium, zirconium, cerium, bismuth, antimony, silicon, tin, and zinc.

With regard to the total weight of the coating that may be formed on the pigment, the limits are not critical; but, as is well-known in the art of surface-treating oxide pigments, a suitable total weight will normally lie in the range of from about 0.5 to about 25%, based on the weight of the uncoated pigment.

The reason why the hydrothermal pressure treatment of coated pigments in accordance with the present invention leads to an improvement in the case of milling of the pigment is not fully understood, but it seems clear that the improvement results from changes in the structure of the surface coating brought about by the treatment process. The structural changes may result from changes in the chemical composition of the coating brought about by the treatment process.

Thus, for example, coatings consisting of one or more hydrous oxides generally have many of the properties of gels and, in consequence, such coatings tend to function as an adhesive during the drying process which

5	normally precedes milling. Adjacent pigmentary particles are bound together by the adhesive action, and relatively intensive milling is required in order to overcome the binding forces, especially when a thick coating has been applied to the pigmentary particles.	70
10	After, drying, coated pigmentary particles that have been treated in accordance with the invention are much less tightly bound together as compared with untreated coated pigment, and it is therefore easier to break down the aggregates by milling. The treatment also tends to densify the coatings, and this leads in turn to the oil absorption value of the finished	75
15	pigment being lower than that of untreated pigment. In general, the filtration rate of the coated pigment and/or the solids content of the resulting filter cake are also improved by the treatment process, although such improvements are not found in the case of certain coatings.	80
20	The structural changes which take place in the coatings can be detected by electron microscopy and are generally accompanied by changes in the solubility of the coating. Thus, for example, the acid solubility of hydrous alumina and of hydrous titania decreases with increasing time at constant pressure and temperature. Further, the time required to produce a given solubility change will, in general, be shorter the higher the temperature and pressure employed.	85
25	The extent to which the structure of the surface coating is modified depends on the composition of the coating, on the pressure and temperature employed during the hydro-thermal pressure treatment, and on the duration of the treatment process. These same parameters also influence the extent to which the oil absorption and gloss values of a coated pigment are altered by the treatment process.	90
30	It will generally be found that, for a treatment of a given duration at pressures of up to about 600 p.s.i.g., the gloss and oil absorption values of the finished pigment will be increasingly good the higher the temperature at which the coated pigment is maintained. Also, it will generally be found that, for a treatment effected at a given temperature and within the same pressure range, there will be a progressive improvement in the gloss and oil absorption of the pigment as the duration of the treatment is increased, although the improvement resulting from prolonging the treatment is not so marked as that resulting from increasing the temperature. Typically, treatment times in the range of from 15 minutes to 2 hours will effect a useful improvement in the gloss and oil absorption values of the pigment. Preferably, the duration of the hydrothermal pressure treatment is at least 30 minutes.	95
35	In the early stages of the treatment, the coating progressively loses its amorphous character and becomes more granular in appear-	100
40	ance; if the treatment is continued, the coating then becomes microcrystalline over the whole of the pigment surface; if the treatment is continued still further, the micro-crystals shrink away from parts of the surface of the particles, and macrocrystals grow on certain sites. Ultimately, the coating consists predominantly of such macrocrystals projecting from the surface of the particles. The macrocrystals are most commonly in the form of platelets, needles, spikes or rods.	105
45	The time required in order to reach any given coating structure decreases with increasing temperature and can decrease, at least in some circumstances, with increasing pressure, and, until the ultimate macrocrystalline stage is reached, the coating structure will change progressively with increasing time at constant pressure and temperature.	110
50	It is found that a coating of hydrous alumina becomes microcrystalline after about 20 minutes at 208°C. and at a total ambient pressure of 250 p.s.i.g. Macrocrystals begin to form in a silica/alumina coating after about 15 minutes at 246°C and 500 p.s.i.g.	115
55	In selecting the temperature and pressure which are to be maintained in order to bring about any particular structural modification of the coating, an allowance should be made for the period of heating up and cooling down the treatment vessel. This allowance is especially important when a large vessel is used, which may take a relatively long period of time to heat up and cool down.	120
60	For those coated pigments of which the photochemical stability is improved by hydro-thermal pressure treatment in accordance with the invention, the extent of the improvement is dependent on the particular conditions employed in the treatment process and on the duration of the process. In the case of pigments having a coating comprising hydrous alumina and hydrous silica, the photochemical stability is greater the longer the treatment process is continued. The term photochemical stability denotes the brightness retention and resistance to yellowing of a paper laminate that incorporates the treated pigment. The time required to reach a given photochemical stability in any particular case is shorter the higher the temperature or pressure involved. After a certain time, however, the photochemical stability remains constant with respect to increased temperature, pressure, or time until, if the process is continued still further, there is a progressive deterioration in the photochemical stability. It has been found that the photochemical stability begins to deteriorate at the onset of the formation of the macrocrystals referred to hereinbefore. Although the treatment conditions required in order to reach this point are very sensitive to changes in the coating parameters, the conditions which give rise to the maximum photochemical stability in any particular case	125
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can be found by routine experiments, as there is a range of conditions over which the photochemical stability is substantially invariant. Moreover, it has been found that some improvement in photochemical stability is obtained at any point before the maximum.

The parameters of the coating which influence the process conditions that lead to the formation of macrocrystals are the nature of the constituents of the coating, the relative proportions of the constituents of a mixed coating, the thickness of the coating and the way in which it has been applied.

Although the light stability of pigments of which the coating has been rendered macrocrystalline tends to be unsatisfactory (and the formation of macrocrystals may lead to a deterioration in the gloss value of the pigment, especially if relatively large crystals are formed), the characteristic crystalline habit of such pigments renders them useful for opacifying paper and in paper coatings.

The hydrothermal pressure treatment in accordance with the invention may be carried out in any suitable pressure vessel, for example, in a stirred autoclave or in an autoclave to which is imparted a rocking or rotating motion. Instead, the treatment may be carried out in a non-agitated autoclave. Thus, for example, an aqueous slurry of pigmentary material may be treated in a stirred vessel, and a thick paste may be treated in a non-agitated vessel. As a further possibility, the pressure treatment may be carried out in a vessel having a constricted outlet to enable a superatmospheric pressure to be established in the vessel; the vessel may be of generally tubular form.

The hydrothermal pressure treatment may be carried out immediately after coating the pigment, that is to say, before washing the coated pigment in order to remove soluble salts. If a conventional autoclave is to be used, it is preferable to remove the soluble salts before treating the coated pigment, as such removal decreases the extent of corrosion of the inner surfaces of the autoclave. On the other hand, the presence of soluble salts can in some cases have a beneficial effect on the crystal habit and defect structure of the treated pigment.

Advantageously, the superatmospheric pressure in the treatment vessel is used to assist in conveying the treated pigment to the next succeeding stage in the manufacture of the final product, possibly as part of a continuous treatment process. For example, if the coated pigment is washed prior to being treated in accordance with the invention, the excess pressure can be used to assist in conveying the pigment to a spray drier.

The invention also provides a paint, paper, or paper laminate that incorporates an oxide pigment that has been treated in accordance with the invention.

The following Examples illustrate the invention:

In each of the Examples, the pressure attained in the pressure treatment vessel was that pressure obtained by sealing in the vessel an aqueous mixture including the coated pigment, and then heating the vessel up to the quoted temperature. Further, it will be seen that, in each Example, the hydrothermal pressure treatment is conducted in the absence of polymerisable monomers.

Example 1.

An aqueous suspension of dry-ground pigmentary titanium dioxide, of which 98.4% was in the rutile crystallographic form was prepared by dispersing 300 grams of the oxide in 1 litre of water in the presence of 0.4% by weight sodium silicate (calculated as SiO_2 and based on the weight of TiO_2) as dispersing agent. Particles larger than 5 microns in diameter were then removed by allowing them to settle out under the action of gravity for an appropriate time and decanting the remaining suspension of fine particles.

The fine titanium dioxide particles in suspension were then coated with a mixture of the hydrous oxides of titanium, silicon and aluminium by adding an aqueous solution of each of titanium sulphate, sodium silicate and aluminium sulphate to the suspension and thereafter adding sufficient caustic soda solution to adjust the pH of the suspension to 7.2. The quantities of titanium sulphate, sodium silicate and aluminium sulphate were sufficient to yield 3.0% hydrous alumina (calculated as Al_2O_3), 3.0% hydrous silica (calculated as SiO_2 and including the 0.4% added as dispersant) and 1.0% hydrous titania (calculated as TiO_2), all the percentages being by weight and based on the weight of titanium dioxide in the initial suspension.

After coating of the pigment, the resulting aqueous slurry was washed to remove soluble salts and then filtered. The wet filter cake, which had a solids content of 51% by weight, was divided into two portions A and B which were treated as described below.

Portion A was dried under atmospheric pressure in a standard laboratory oven for 16 hours at 110°C.

Portion B was contacted with water in an autoclave for 1 hour at 185°C., the total pressure in the autoclave being 150 pounds per square inch gauge (p.s.i.g.). After cooling of the treated pigment, it was dried in the same manner as described above for portion A.

Each of the two dried portions, A and B, was then tested in an emulsion paint formulation and in a paper laminate formulation.

The emulsion paint test was carried out as follows:

A known standard weight of the pigment was stirred into a known standard quantity

of a solution of a hydroxyl alkyl cellulose thickener until the pigment was thoroughly wetted. The viscosity of the resulting emulsion was measured, and the changes in viscosity on adding successive quantities of tetrox ("Tetron" is a Trade Mark) was observed until there was no further change in viscosity. The amount of tetrox required in order to attain this limiting viscosity is a measure of the ease 10 of dispersibility of the pigment. The results of this test are shown in the following Table, which also shows the hiding power, in square feet per imperial gallon, of an air-drying

acrylic resin paint containing 37% by weight of the pigment. The hiding power was determined by the method described in the American Society for Testing Materials publication D 1738-60T, issued in 1960, with the substitution of Imperial gallons for U.S. gallons where appropriate. The hiding power is therefore the number of square feet over which an Imperial gallon of paint can be uniformly spread to produce a contrast ratio $C=0.98$, the contrast ratio being defined in the ASTM publication.

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	Initial viscosity	Final viscosity	Amount tetrox required	Hiding power
Portion A	8.6	0.8	0.05	472
Portion B	2.4	0.8	0.03	565

It can be seen from the above Table that the dispersibility and hiding power of portion B, which had been obtained in accordance 30 with the invention, is superior to that of portion A.

The paper laminate test was carried out as follows:

Paper laminates incorporating the pigment 35 were prepared using a water-soluble amino formaldehyde condensate resin binder and were exposed to Xenon radiation in a laboratory weatherometer for 24 hours. Before and after exposure the laminates were tested using

a Colormaster differential colorimeter. The brightness and whiteness of each laminate on the Adams Chromatic Value System are given in the Table below. In the Adams system, "L" represents a logarithmic function of the brightness, referred to a smoked magnesium oxide surface (for which $L=100$) and "b" represents the degree of yellowness of the light reflected (the value for magnesium oxide being zero). It is desirable to have as high an "L" value as possible, and a "b" value 40 as near to zero as possible.

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	Before exposure "L"	After exposure "L"	ΔL	Δb
	"b"	"b"		
A	91.34	+1.5 81.82	-0.7	-9.52 -2.2
B	90.1	+1.5 84.55	+0.7	-5.55 -0.8

It can be seen from the above Table that the photochemical stability of portion B is 55 superior to that of portion A.

Example 2.

800 grams of pigmentary titanium dioxide that had been obtained by the vapour phase oxidation of titanium tetrachloride were suspended in 1 litre of water in the presence of 60 0.25% by weight of tetra sodium pyrophosphate (based on the weight of TiO_2) as dispersing agent. The pH of the suspension was adjusted to 10.0 with caustic soda solution.

The suspension was then sand-milled for 65 15 minutes in a laboratory sand mill of the batch type. After sieving the milled suspension, residual sand and any titanium dioxide particles larger than 5 microns were 70 removed by allowing them to settle out under the action of gravity for the appropriate calculated period and then decanting the remaining suspension of fine particles.

The fine titanium dioxide particles were 75 then coated with hydrous titania and hydrous

alumina by adding a quantity of titanyl aluminium sulphate solution to the suspension (the ratio by weight $TiO_2 : Al_2O_3$ in the said solution being 1.0:1.5) and thereafter precipitating the hydrous oxides by adding ammonium hydroxide until the pH of the suspension was 7.5. The amount of titanyl aluminium sulphate added was equivalent to 2% by weight of TiO_2 and 3% by weight of Al_2O_3 , based on the titanium dioxide content of the suspension.

The resulting aqueous slurry was then divided into four equal parts. Three of these parts were subjected to the different hydro-thermal pressure treatments in accordance with the invention shown in the Table below. After being treated, the pigment slurry was washed with demineralised water to remove soluble salts and filtered, and the resulting filter cake was then dried in a laboratory oven for 16 hours at $120^\circ C$. The dried filter cakes were then crushed to a size suitable for feeding to a laboratory-scale fluid

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energy mill, which was operated on air. Each of the crushed pigments was then milled under the same conditions of feed rate, jet pressure and ring pressure.

5 In order to provide a basis for comparison, the four part of the aqueous slurry of the coated pigment was washed, filtered, dried and milled as described above, but without having been subjected to any hydrothermal pressure treatment.

10 The oil absorption value of each of the four samples of milled pigment was measured,

and the pigments were then incorporated into an air-drying acrylic resin medium to the extent of 37% by weight in each case. The percentage gloss values of the resulting paints were measured as described in British Patent Specification No. 1,155,567, and the results obtained are shown in the following Table, which also shows the oil absorption value of the milled pigment. It is desirable to have as high a percentage gloss and as low an oil absorption as possible.

Part No.	Hydrothermal Treatment	Oil absorption	Percentage Gloss
1	4 hrs. at 100 psig and 167.5°C.	17.5	75
2	2 hrs. at 200 psig and 197.5°C.	16.3	73
3	30 mins. at 2,000 psig and 335°C.	15.5	68
4	None	18.9	60

25 Example 3.

A quantity of rolled pigmentary TiO_2 , that had been obtained by the sulphate process, and of which 98.5% was in the rutile form, was leached with demineralised water

30 for 30 minutes at 70°C. The leached material was then filtered and washed to reduce its water-soluble content to a low level. An aqueous slurry of the washed pigment having a concentration of 400 gm.

35 TiO_2 /litre was then prepared by dispersing the pigment in water at pH 10.2 in the presence of 0.25% by weight of sodium tetraphyrophosphate as dispersing agent. A coating comprising hydrous alumina and hydrous titania was then applied to the pigmentary particles in the following manner at room temperature.

40 3% by weight of aluminium sulphate (calculated as Al_2O_3 and based on the weight of TiO_2) was added to the pigment slurry in the form of an aqueous solution containing the equivalent to 100 gms. Al_2O_3 /l. This addition reduced the pH of the slurry to 3.2.

45 Hydrous alumina incorporating some basic aluminium sulphate was then precipitated onto the titanium dioxide particles by adding sodium hydroxide solution to the slurry with stirring until the pH was 7.0. 2% by weight of titanium tetrachloride (calculated as TiO_2 ,

50 and based on the weight of TiO_2 initially present in the slurry) was added to the slurry of the alumina-coated pigment over a period of 15 minutes, and the slurry was then stirred for a further 15 minutes, after which time its pH was 3.8 and 42% of the hydrous alumina had been dissolved. The titanium tetrachloride was added to the slurry in the form of a

chloride was added to the slurry in the form of a solution containing the equivalent of 160 gms. TiO_2 per litre, and substantially the whole of the titanium tetrachloride was precipitated as hydrous titania.

55 The dissolved alumina was then reprecipitated onto the pigmentary particles by the addition of sodium hydroxide solution over a period of 30 minutes to give a final pH of 7.2. The resulting slurry was filtered and the filter cake so obtained was divided into thirteen equal parts. Twelve of these parts were subjected to the different hydrothermal pressure treatment in accordance with the invention and shown in the Table below. After being treated, the pigment was washed with demineralised water to remove soluble salts and filtered, and the resulting filter cake was

60 then dried in a laboratory oven for 16 hours at 120°C. The dried filter cakes were then crushed to a size suitable for feeding to a laboratory scale fluid energy mill, which was operated on air. Each of the crushed pigments was then milled under the same conditions of feed rate, jet pressure and ring pressure.

65 In order to provide a basis for comparison, the thirteenth part of the initial filter cake was washed, filtered, dried and milled as described above, but without having been subjected to any hydrothermal pressure treatment.

70 As described in Example 2, the oil absorption value of each of the thirteen samples of milled pigment, and the percentage gloss of paints incorporating the pigments, were measured. The results are included in the following Table.

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Part No.	Hydrothermal Treatment	Oil absorption	Gloss
1	15 mins. at 150°C. (corresponding to 55 psig)	18.7	67
2	30 mins. at 150°C. (corresponding to 55 psig)	18.7	70
3	60 mins. at 150°C. (corresponding to 55 psig)	18.7	72
4	120 mins. at 150°C. (corresponding to 55 psig)	18.7	70
5	15 mins. at 200°C. (corresponding to 210 psig)	17.5	71
6	30 mins. at 200°C. (corresponding to 210 psig)	18.4	75
7	60 mins. at 200°C. (corresponding to 210 psig)	17.5	73
8	120 mins. at 200°C. (corresponding to 210 psig)	17.8	76
9	15 mins. at 250°C. (corresponding to 580 psig)	16.6	75
10	30 mins. at 250°C. (corresponding to 580 psig)	17.5	77
11	60 mins. at 250°C. (corresponding to 580 psig)	17.2	75
12	120 mins. at 250°C. (corresponding to 580 psig)	16.0	76
13	None	20.3	65

Example 4.

5 An aqueous dispersion of pigmentary titanium dioxide was prepared as described in Example 3. The pigmentary particles were then coated with hydrous alumina and hydrous titania as described below.

10 Aluminium sulphate solution equivalent to 5% by weight of Al_2O_3 (based on the weight of TiO_2) was added to the dispersion thereby reducing its pH to 3.4. Hydrous alumina incorporating some basic aluminium sulphate was then precipitated onto the pigment by adding sodium hydroxide solution to the slurry over a period of 15 minutes until a pH of 8.0 was attained. After precipitation, a quantity of titanium tetrachloride (165 gm. TiO_2/l) equivalent to 2% by weight of TiO_2 was added to the slurry over a period of 10 minutes. The pH of the resulting slurry was

3.6 and 76% of the hydrous alumina had been dissolved. At the same time substantially the whole of the added titanium tetrachloride had been precipitated as hydrous titania. The pH of the acidic slurry was then raised to 8.0 by the addition of sodium hydroxide solution, causing re-precipitation of the hydrous alumina that had been dissolved in the previous step. The resulting coated particles were then isolated by filtration and the filter cake so obtained was divided into four parts. Three of the parts were hydrothermally treated for 30 minutes at 150, 200 and 250°C. respectively, and the treated pigments were washed, filtered, dried and milled, as described in Example 3.

25 30 35 In order to provide a basis for comparison, the fourth part of the initial filter cake was washed, filtered, dried and milled under the

same conditions as the other three parts, but without having been subjected to any hydro-thermal pressure treatment.

As described in Example 3, oil absorption and gloss values were measured, and the results are set out in the following Table: 5

Part No.	Hydrothermal Treatment	Oil absorption	Gloss
1	30 mins. at 150°C. (corresponding to 55 psig)	22.4	62
2	30 mins. at 200°C. (corresponding to 210 psig)	19.7	70
3	30 mins. at 250°C. (corresponding to 580 psig)	16.9	76
4	None	23.1	53

Example 5.

10 A disperse aqueous slurry of titanium dioxide pigment was prepared as described in Example 3, and the pigmentary particles were then coated with hydrous alumina and hydrous zirconia as described below.

15 Aluminium sulphate solution equivalent to 3% by weight of Al_2O_3 (based on TiO_2) was added to the disperse slurry, thereby reducing its pH to 3.3. Hydrous alumina incorporating some basic aluminium sulphate was then precipitated onto the pigmentary particles by 20 adding ammonium hydroxide solution to the slurry over a period of 15 minutes until a pH of 6.0 was attained. After precipitation, a quantity of zirconium oxychloride solution (80 gm. ZrO_2/l) equivalent to 2% by 25 weight of ZrO_2 (based on the weight of TiO_2) was added to the slurry over a period of 10 minutes. The pH of the resulting slurry was 3.7 and 67% of the hydrous alumina had been dissolved. At the same time substantially the whole of the added zirconium 30

oxychloride had been precipitated as hydrous zirconia. The pH of the acidic slurry was then raised to 8.0 by the addition of ammonium hydroxide solution, causing reprecipitation of the hydrous alumina that had been dissolved in the previous step. The resulting slurry was then filtered and the filter cake obtained was divided into ten parts, nine of which were subjected to the different hydrothermal pressure treatments shown in the Table below. As described in Example 3, the treated pigments were washed, filtered, dried and milled. 35

40 In order to provide a basis for comparison, the tenth part of the initial filter cake was washed, filtered, dried and milled under the same conditions as the other nine parts, but without having been subjected to any hydro-thermal pressure treatment. 45

45 As described in Example 3, oil absorption and gloss values were measured, and the results are set out in the following Table: 50

Part No.	Hydrothermal Treatment	Oil absorption	Gloss
1	15 mins. at 150°C. (corresponding to 55 psig)	20.0	62
2	30 mins. at 150°C. (corresponding to 55 psig)	20.3	66
3	60 mins. at 150°C. (corresponding to 55 psig)	19.7	68
4	15 mins. at 200°C. (corresponding to 210 psig)	19.4	68
5	30 mins. at 200°C. (corresponding to 210 psig)	19.1	70
6	60 mins. at 200°C. (corresponding to 210 psig)	18.4	71
7	15 mins. at 250°C. (corresponding to 580 psig)	18.4	75
8	30 mins. at 250°C. (corresponding to 580 psig)	18.7	76
9	60 mins. at 250°C. (corresponding to 580 psig)	18.7	73
10	None	19.1	68

5 After the hydrothermal pressure treatment processes, the pigment coatings were examined under the electron microscope at a magnification of 150,000. It was found that the coatings of parts 1 to 5 were generally amorphous, and appeared very similar to the coating of part 10, which had not been hydrothermally treated.

10 The coating of part 6 showed the presence of some microcrystals in the form of spikes, and part 7 was very similar. In the coatings of parts 8 and 9, the crystals were somewhat larger, and some bare patches were observed, indicating that the coating had shrunk away from certain sites.

Example 6.

20 An aqueous slurry of rolled and leached titanium dioxide pigment, that had been prepared by the sulphate process, was prepared by dispersing the pigment in water in the presence of 0.25% by weight of tetrone as dispersing agent. The pigment concentration in the slurry was 240 grams/litre. 6% by weight of magnesium sulphate (calculated as MgO and based on the weight of TiO₂) was slowly added to the pigment slurry in the form of an aqueous solution containing the equivalent of 80 gm MgO/l. The slurry was

then heated to 80° C. and maintained at this temperature for 30 minutes, after which time the pH was adjusted to 10 by the addition of 10N sodium hydroxide, so precipitating magnesium hydroxide onto the pigmentary particles. The resulting slurry was filtered while still hot.

30 One third of the filter cake so obtained was then subjected to hydrothermal pressure treatment in an autoclave for two hours at 185° C. The treated pigment was allowed to cool slowly and was then washed, filtered, dried, and milled, as described in Example 3, to yield a finished pigment I.

35 The remaining two-thirds of the filter cake was washed and was then slurried in one litre of water and filtered. The slurry so obtained was filtered, and the filter cake was then slurried and filtered twice: the filter cake finally obtained was divided into two portions. One portion was subjected to hydrothermal pressure treatment in an autoclave for two hours at 185° C. The treated pigment was allowed to cool slowly and was then dried and milled to yield a finished pigment II.

40 In order to provide a basis for comparison, the second portion of the washed filter cake was dried and milled under the same con-

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ditions as were employed for pigments I and II, but without having been subjected to any hydrothermal pressure treatment.

As described in Example 2, the oil absorption value of each of pigments I to III, and the percentage gloss of paints incorporating the pigments, were measured. The results were as follows:

10	Sample	Gloss	Oil
			Absorption
	1	39	20.6
	2	38	20.9
	3	24	24.4

It can be seen from these results that an improvement in the gloss and oil absorption values of the pigment was obtained both when the coated pigment was washed prior to being subjected to hydrothermal pressure treatment (pigment II), and when the washing was not carried out until after the treatment process.

Example 7.

Four samples of finished titanium dioxide pigment were prepared as described below.

Titanium dioxide pigment was coated with 3% by weight of hydrous alumina (calculated as Al_2O_3) and 2% by weight of hydrous titania (calculated as TiO_2) as described in Example 3. One portion of the coated pigment was subjected to hydrothermal pressure treatment for 30 minutes at 195°C. (corre-

ponding to 200 p.s.i.g.), and was then washed, dried, and milled in a fluid-energy mill to yield a finished pigment I. In order to provide a basis for comparison, a further portion of the coated pigment was washed, dried and milled under the same conditions to yield a finished pigment II, but without being subjected to hydrothermal pressure treatment.

Titanium dioxide pigment was coated with hydrous alumina and hydrous titania as described in Example 4, except that the proportion of hydrous titania was 1% by weight, instead of 2% by weight as described in that Example. One portion of the coated pigment was subjected to hydrothermal pressure treatment for 30 minutes at 195°C. (corresponding to 200 p.s.i.g.), and the treated pigment was then washed, dried and milled under the same conditions as samples I and II, to yield a finished pigment III. In order to provide a basis for comparison, a further portion of the coated pigment was washed, dried and milled under the same conditions, but without having been subjected to any hydrothermal pressure treatment. The resulting finished pigment was designated IV.

The brightness and whiteness of each of pigments I to IV, and of air-drying alkyd paid media incorporating the pigments, were then measured on the Adams Chromatic Value System (see Example 1). The "L" and "b" values so obtained are set out in the following table.

Pigment	Pigment alone		Air-drying alkyd medium		Δb
	"L"	"b"	"L"	"b"	
I	97.3	+2.0	94.2	+3.6	+1.6
II	97.4	+2.0	94.2	+4.5	+2.5
III	97.2	+2.2	94.2	+3.6	+1.6
IV	97.5	+2.0	94.1	+4.2	+2.2

It can be seen from the above table that the increase in yellowing resulting from incorporating the pigment into an alkyd medium was relatively less for those pigments that had been subjected to hydrothermal pressure treatment.

Example 8.

A quantity of titanium dioxide pigment that had been prepared by the vapour-phase oxidation of titanium tetrachloride was dispersed in water and the resulting dispersion was heated to 60°C. Sodium phosphate solution (containing the equivalent of 25.0 g phosphorus pentoxide per litre) and aluminium sulphate solution (containing the equivalent of 100 g aluminium oxide per

litre) was added simultaneously to the dispersion over a period of 45 minutes until 2% by weight P_2O_5 (based on TiO_2) and 1.5% by weight Al_2O_3 (based on TiO_2) were present. The pH of the dispersion was adjusted to 6 by the addition of sodium hydroxide solution over a period of 30 minutes and the resulting slurry was then stirred for a further 30 minutes. The phosphate-coated pigment was then recovered by filtration and the filter cake was washed and divided into two portions.

One portion of the filter cake was subjected to hydrothermal pressure treatment for one hour in an autoclave at 185°C. (150 p.s.i.g.). After being allowed to cool, the

treated pigment was dried in a laboratory oven for 16 hours at 110° C. to yield pigment A.

5. The other portion of the filter cake was dried in the same manner as described for portion A, to yield pigment B.

Each of the two dried portions A and B was tested in a paper laminate formulation as described in Example 1, and the following results were obtained.

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	Before Exposure		After Exposure		ΔL	Δb
	"L"	"b"	"L"	"b"		
A	90.1	+1.3	86.2	+0.9	-3.9	-0.4
B	90.6	+1.3	82.7	-0.3	-7.9	-1.6

It can be seen from the above table that the photochemical stability of portion A was superior to that of portion B.

15. WHAT WE CLAIM IS:—

1. A process for the treatment of an oxide pigment, which comprises forming on the pigment a coating comprising at least one substance selected from hydroxides, hydrous oxides, phosphates and basic sulphates of beryllium, calcium, magnesium, barium, boron, aluminium, silicon, tin, lead, antimony, titanium, zirconium, hafnium, niobium, tantalum, zinc, and cerium, and subjecting the 20 coated pigment to hydrothermal pressure treatment by maintaining it at a temperature of at least 50° C. in the presence of liquid water and with a total ambient pressure exceeding one atmosphere.
2. A process as claimed in claim 1, wherein there is liquid water in contact with the coated pigment during the hydrothermal pressure treatment.
3. A process as claimed in claim 1 or claim 2, wherein the superatmospheric pressure is the pressure obtained when an aqueous mixture including the coated pigment is sealed in a closed vessel and thereafter heated to the desired temperature.
4. A process as claimed in claim 1 or claim 2, wherein a quantity of a gas is introduced into the treatment vessel to augment the ambient pressure.
5. A process as claimed in claim 4, wherein the gas is air or nitrogen.
6. A process as claimed in any one of claims 1 to 5, wherein the coated pigment is maintained at a temperature of at least 150° C.
50. 7. A process as claimed in any one of claims 1 to 6, wherein the amount of water in the pressure treatment vessel and the conditions of temperature and pressure therein are such that substantially the whole of the exposed surface area of the coated pigment is in contact with liquid water.
55. 8. A process as claimed in any one of claims 1 to 7, wherein the duration of the hydrothermal pressure treatment is at least 15 minutes.

9. A process as claimed in any one of claims 1 to 7, wherein the duration of the hydrothermal pressure treatment is at least 30 minutes.

10. A process as claimed in any one of claims 1 to 9, wherein the duration of the hydrothermal pressure treatment does not exceed 2 hours.

11. A process as claimed in any one of claims 1 to 10, wherein the hydrothermal pressure treatment is conducted in the absence of polymerisable monomers.

12. A process as claimed in any one of claims 1 to 11, wherein the coated pigment is washed prior to being subjected to the hydrothermal pressure treatment.

13. A process as claimed in any one of claims 1 to 12, wherein the superatmospheric pressure in the pressure treatment vessel is used to assist in conveying the hydrothermally-treated pigment to apparatus for carrying out a further process step.

14. A process as claimed in claims 12 and 13, wherein the superatmospheric pressure is used to convey the hydrothermally-treated pigment to a spray drier.

15. A process as claimed in any one of claims 1 to 14, wherein the hydrothermal pressure treatment is carried out in a stirred autoclave.

16. A process as claimed in any one of claims 1 to 14, wherein the hydrothermal pressure treatment is carried out in an autoclave to which is imparted a rocking or rotating motion.

17. A process as claimed in any one of claims 1 to 14, wherein the hydrothermal pressure treatment is carried out in a non-agitated vessel.

18. A process as claimed in any one of claims 1 to 17, wherein the pigment is coated with one or more substances selected from hydroxides, hydrous oxides, and basic sulphates.

19. A process as claimed in any one of claims 1 to 18, wherein some or all of the constituents of the pigment coating are formed by acid-base reactions.

20. A process as claimed in any one of

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claims 1 to 18, wherein some or all of the constituents of the pigment coating are formed by hydrolytic reactions.

21. A process as claimed in any one of claims 1 to 20, wherein the pigment is coated with hydrous oxides of titanium, aluminium, and silicon.

22. A process as claimed in any one of claims 1 to 20, wherein the pigment is coated with hydrous oxides of titanium and aluminium.

23. A process as claimed in any one of claims 1 to 20, wherein the pigment is coated with hydrous alumina and hydrous zirconia.

24. A process as claimed in any one of claims 1 to 17, wherein the pigment coating consists of or includes a phosphate, of titanium, aluminium, or zirconium.

25. A process as claimed in claim 18, wherein the coating is formed by precipitating quantities of hydroxides or hydrated oxides of two or more of aluminium, silicon, boron, titanium, antimony, zinc, magnesium, tin, lead, cerium and zirconium into intimate association with the pigment.

26. A process as claimed in any one of claims 1 to 24, wherein the pigment coating consists of one layer formed by co-precipitation of two or more substances selected from

hydroxides, hydrated oxides, phosphates, and basic sulphates.

27. A process as claimed in any one of claims 1 to 24, wherein the pigment coating comprises a plurality of discrete layers, each of which is deposited separately. 35

28. A process as claimed in claim 27, wherein each discrete layer consists of a single substance.

29. A process as claimed in claim 27, wherein some or all of the layers consist of more than one substance. 40

30. A process as claimed in any one of claims 1 to 29, wherein the oxide pigment is a titanium dioxide pigment. 45

31. A process as claimed in claim 30, conducted substantially as described in any one of the Examples herein.

32. An oxide pigment whenever treated by a process as claimed in any one of claims 1 to 31. 50

33. A paint, paper, or paper laminate that incorporates an oxide pigment as claimed in claim 32.

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